

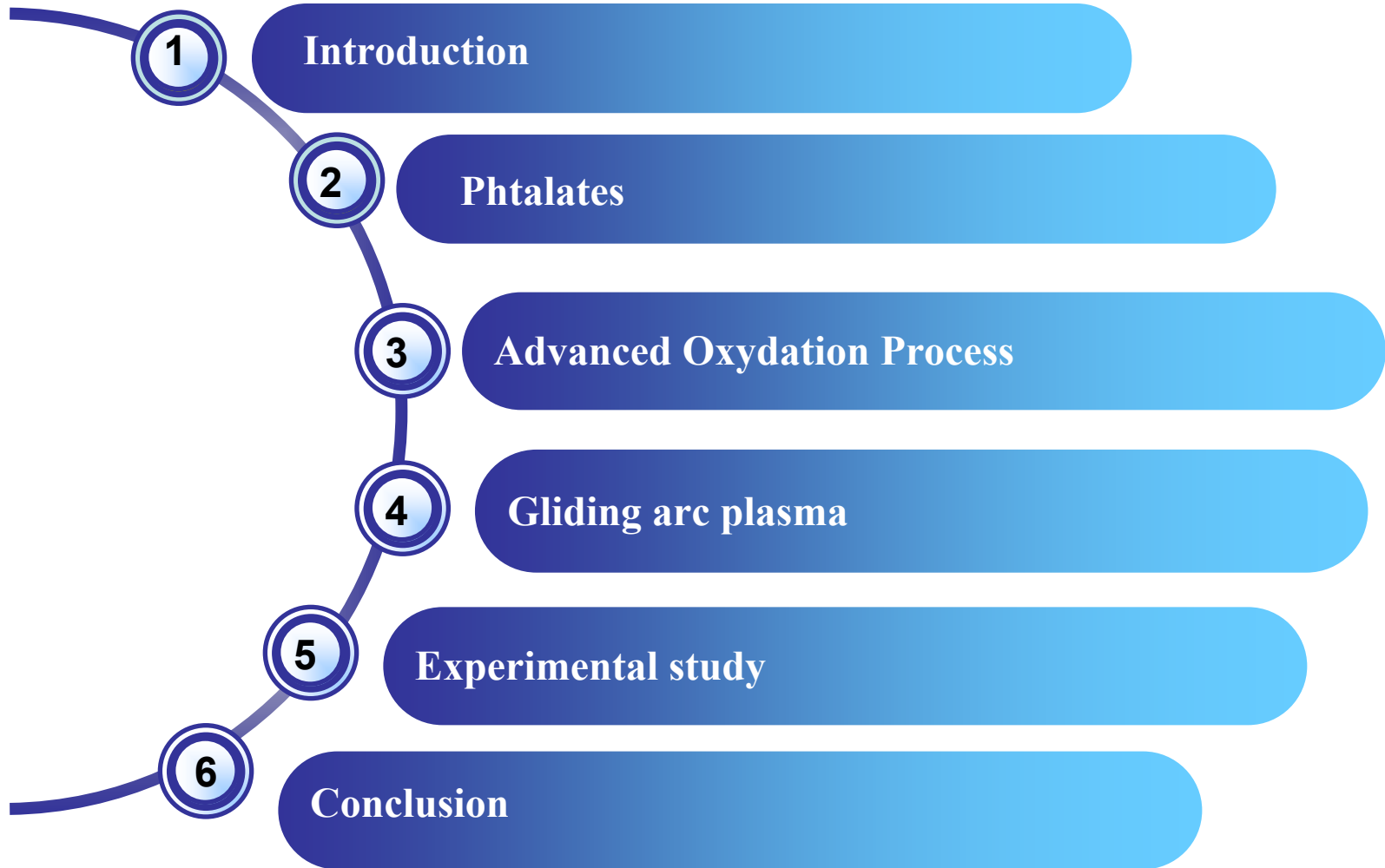


Plasma chemical oxidation of phthalic anhydride: Application to the treatment of Tunisian landfill leachate

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Plan





The increase of industrial and agricultural activities in developing countries



The use of high varieties of synthetic chemicals



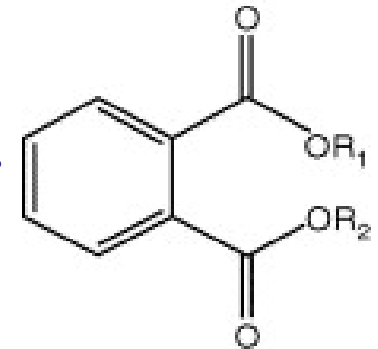
Synthetic chemicals are considered toxic when they are present in aquatic environment



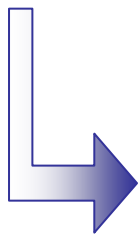
80% of the diseases are directly associated with polluted water.



1,2-dicarboxylic benzene acids + Alcohol \leftrightarrow Phtalates + water



- They are essentially used as plasticizers to increase the flexibility and durability of polyvinyl chloride
- Several industrial plants produce large amounts of wastewater containing high concentration of phthalates (COT = 6400,88 mg L⁻¹).



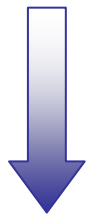
The need to develop an effective, ecological and economical treatment processes becomes obvious



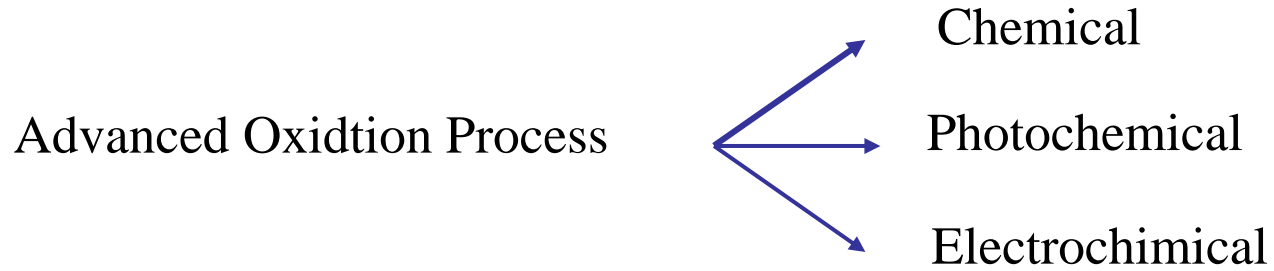
Removal of Phthalates \longrightarrow Biological Process



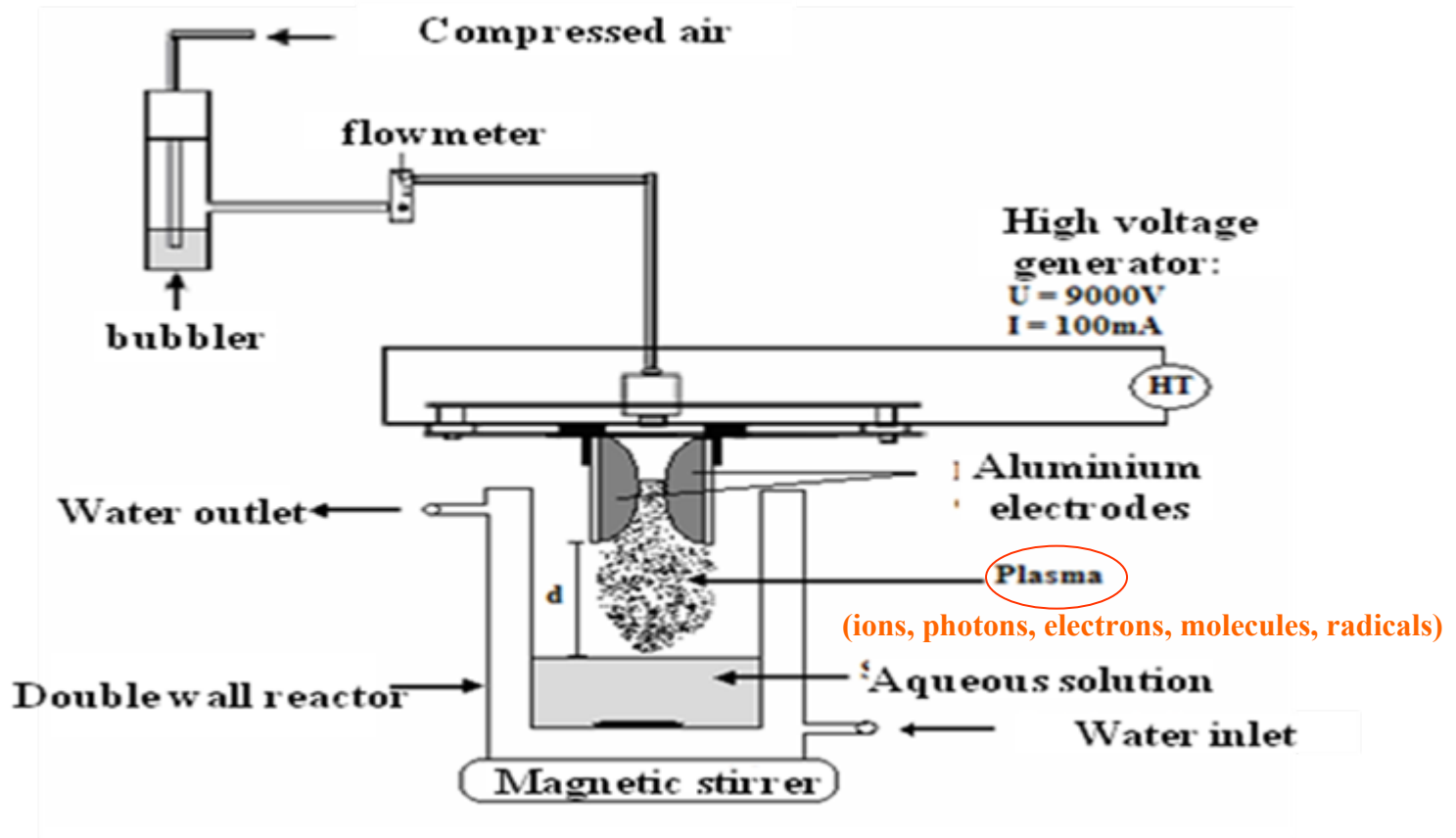
Advanced Oxidation Process (AOP) \longleftarrow Insuffisient



In situ generation of hydroxyl radical : $\cdot\text{OH}$ ($E^\circ_{\text{OH}\cdot/\text{H}_2\text{O}}=2,8 \text{ V/ENH}$)

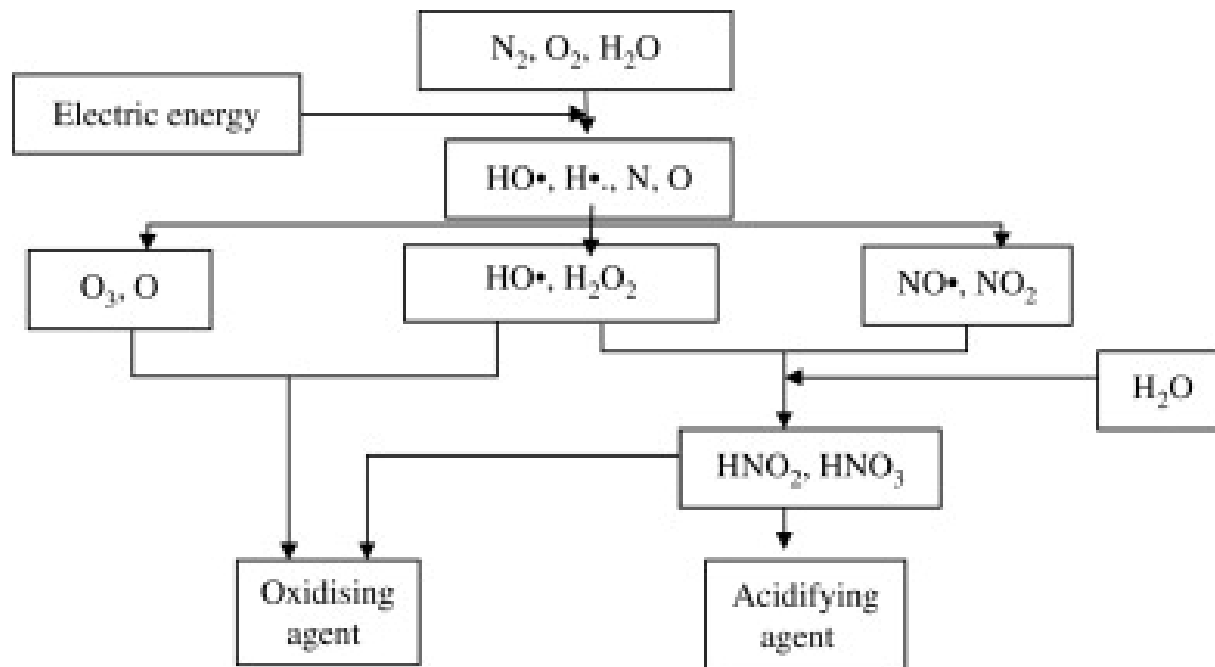


Gliding arc discharge « Glidarc »





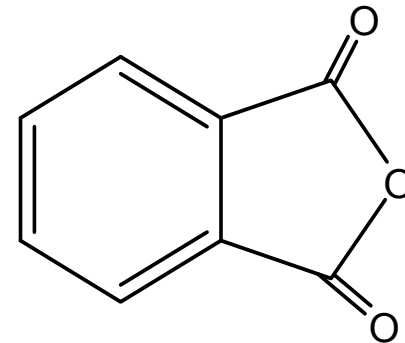
Chemical properties of Glidarcs





The Gliding arc plasma depends on several factors

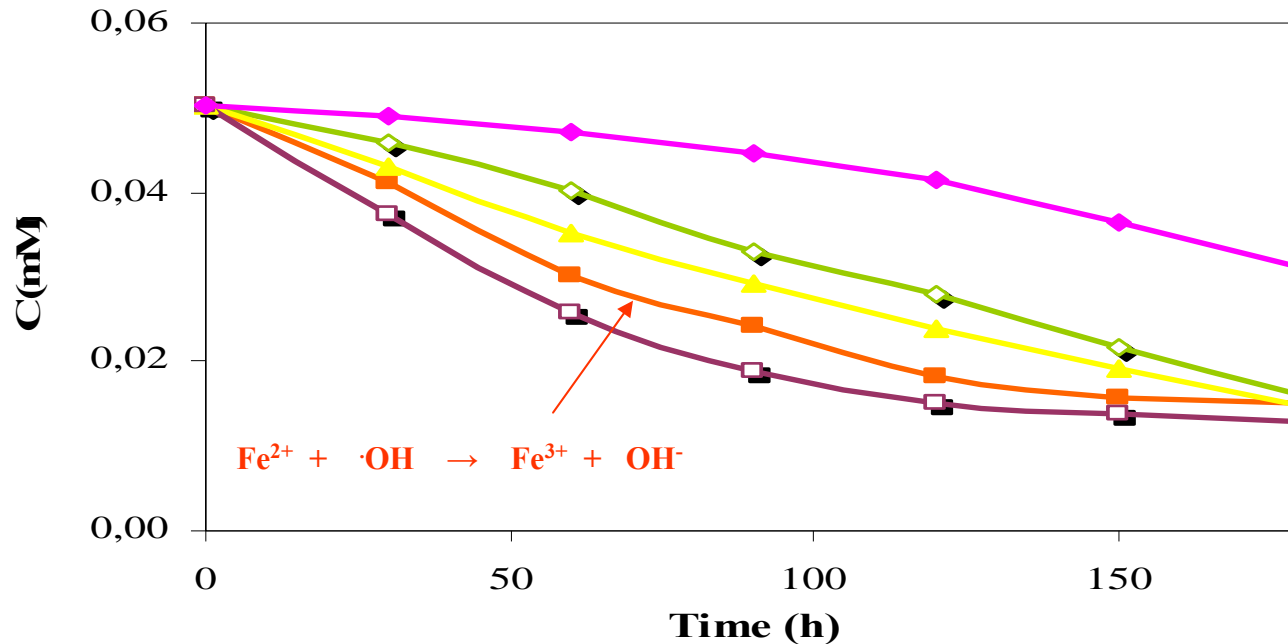
- ➡ **The nature of catalyst**
- ➡ **The catalyst initial concentration**



Phthalic anhydride



Effect of the Fe^{2+} initial concentration

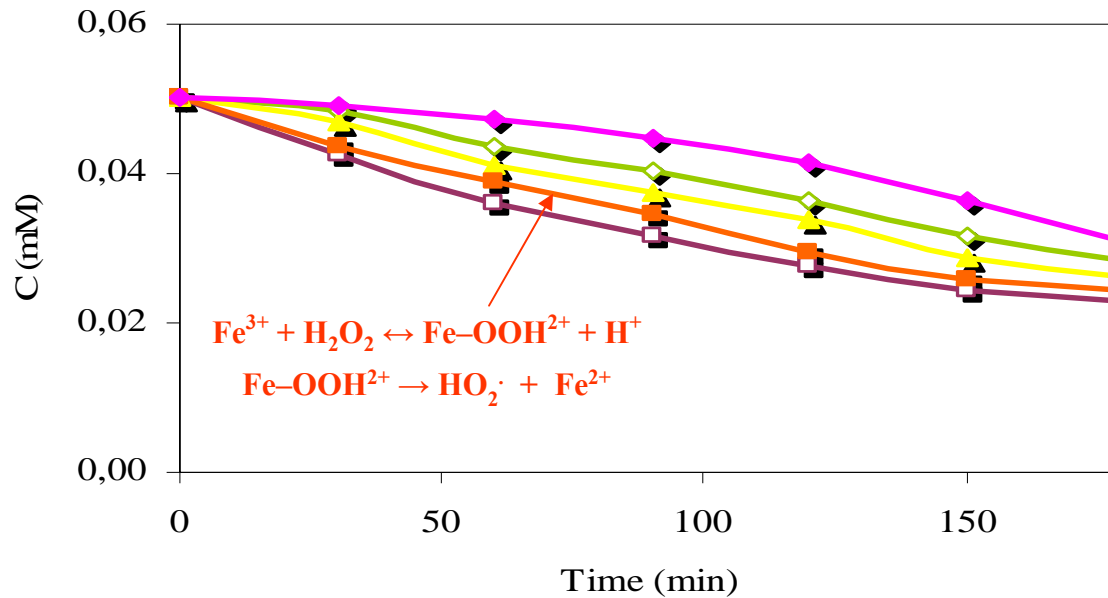


$[\text{Fe}^{3+}]_0$: 0 mM (◆); 0,1 mM (◇); 0,2 mM (▲), 0,5 mM (□), 1 mM (■)

$[\text{phthalic anhydride}]_0 = 0,05 \text{ mM}$, $V = 200 \text{ mL}$, $\Phi = 650 \text{ L h}^{-1}$, $d = 2,5 \text{ cm}$.



Effect of the Fe^{3+} initial concentration

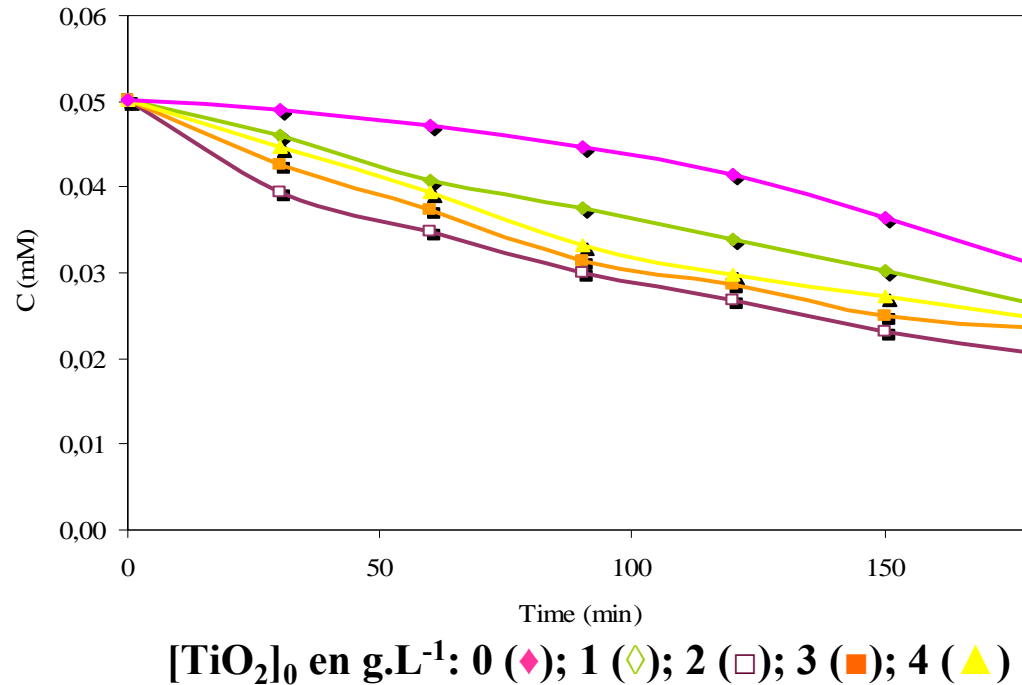


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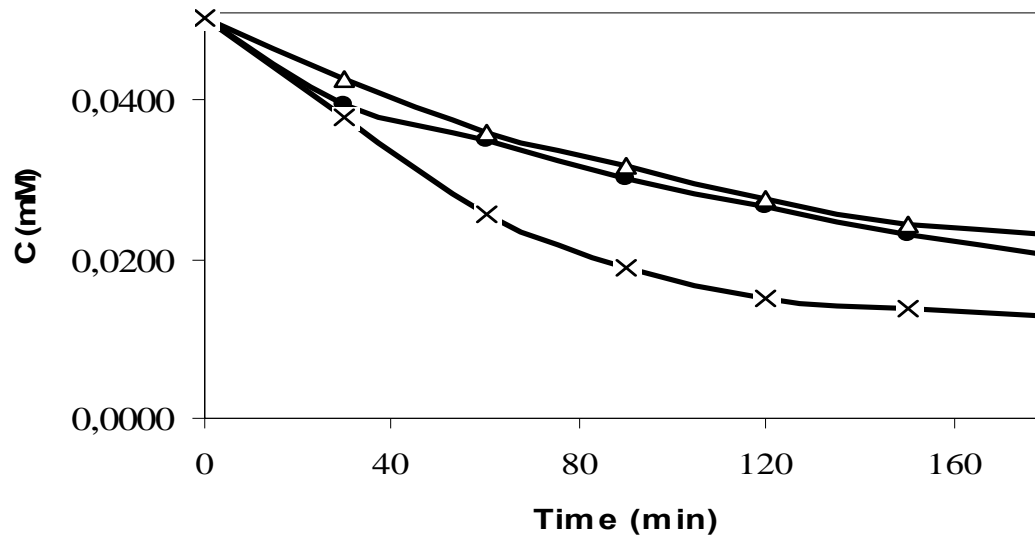
Plasmachemical treatment with TiO_2



$[\text{phthalic anhydride}]_0 = 0,05 \text{ mM}$, $V = 200 \text{ mL}$, $\Phi = 650 \text{ L h}^{-1}$, $d = 2,5 \text{ cm}$.



Study of the efficiency of catalysts



[Fe²⁺] = 0,5 mM (x); [Fe³⁺] = 0,5 Mm (Δ); [TiO₂] = 2 g.L⁻¹ (•)

[phthalic anhydride]₀ = 0,05 mM, V = 200 mL, Φ = 650 L h⁻¹, d = 2,5 cm.

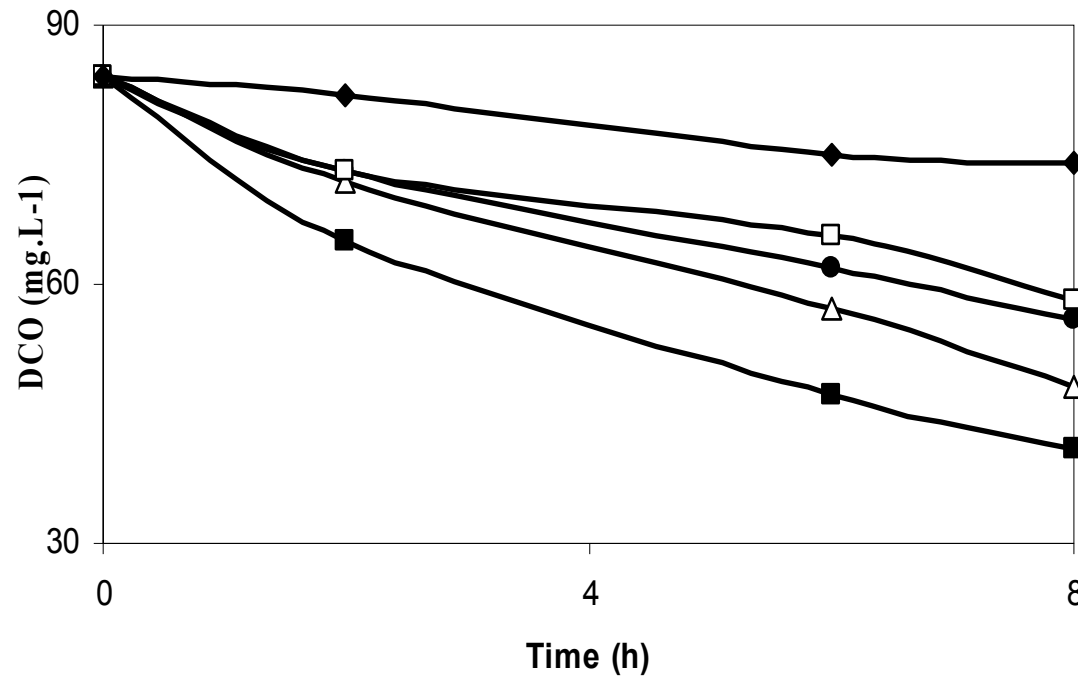


Characteristics of Tunisian landfill leachate

parameters	value
COD_0 (mg/L)	10200
pH	8.15
Conductivity (mS.cm ⁻²)	39.7 à 22.8°C
[Fe] (mmol/L)	0.135



Plasmacatalysis depollution of landfill leachate with TiO_2

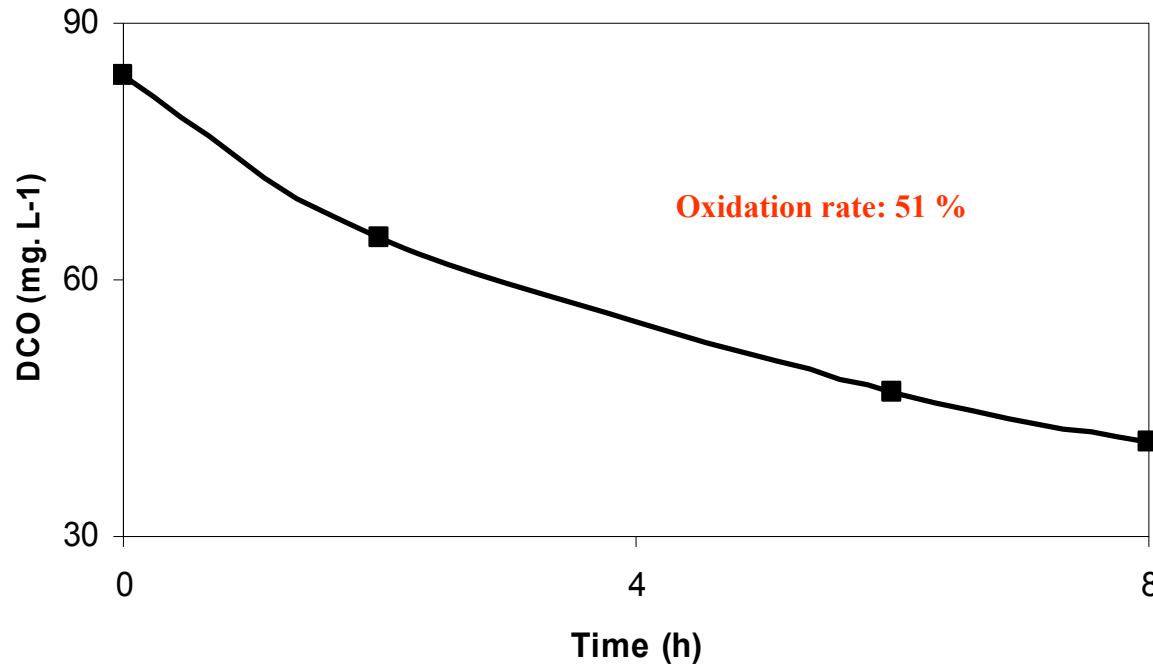


$[\text{TiO}_2]$ en g L^{-1} : 0 (●); 10 (Δ); 15 (■); 25 (□) and 35 (◆).

$[\text{phthalic anhydride}]_0 = 0,05 \text{ mM}$, $V = 200 \text{ mL}$, $\Phi = 650 \text{ L.h}^{-1}$, $d = 2,5 \text{ cm}$.





Plasmacatalysis depollution of landfill leachate under optimum conditions



$[\text{phthalic anhydride}]_0 = 0,05 \text{ mM}$, $[\text{TiO}_2]_0 = 15 \text{ g.L}^{-1}$, $V = 200 \text{ mL}$,
 $\Phi = 650 \text{ L.h}^{-1}$, $d = 2,5 \text{ cm}$.



 **Gliding arc discharge**  **Oxidation rate = 75 %**

Effeciency of this method in removing phtalates from Tunisian landfill leachate:
Oxidation rate = 51%.

 The disadvantage of this technique is the electrical energy consumed .



Thanks for your attention